

# FLUENT in Intermediate Fluid Dynamics

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## MOTIVATION

- Computer-based simulation has become an integral part of engineering practice of fluid dynamics.

⇒ The intelligent and proper use of CFD tools is an important engineering skill to be imparted at the undergraduate level.

- Scientific knowledge is encapsulated in CFD tools.

⇒ Easy-to-use CFD software offers the opportunity to improve and enrich students' understanding of fundamental concepts.

## OBJECTIVES

FLUENT introduced in *M&AE 423/523 Intermediate Fluid Dynamics* in Spring '02. Taught by Prof. Lance Collins.

- Expose students to the intelligent use of an industry-standard CFD tool.
- Use FLUENT as a platform for students to explore flow physics and to reinforce fundamental concepts.
- Use hands-on simulations and a rich visual medium to stimulate student interest and facilitate learning.

## FLUENT VS. FLOWLAB

- FLOWLAB: Wrapper around FLUENT which makes it easier for students to run simulations by limiting available options.
- Considered using FLOWLAB in *M&AE 423* but decided FLUENT was more appropriate.
  - More useful for students to be exposed to a full-fledged CFD package at this level.
  - FLOWLAB results were not validated adequately at that point.

Provided the geometry and grid for running FLUENT.

FLOWLAB is more appropriate in an introductory-level class and/or lab.

## FLUENT EXAMPLES

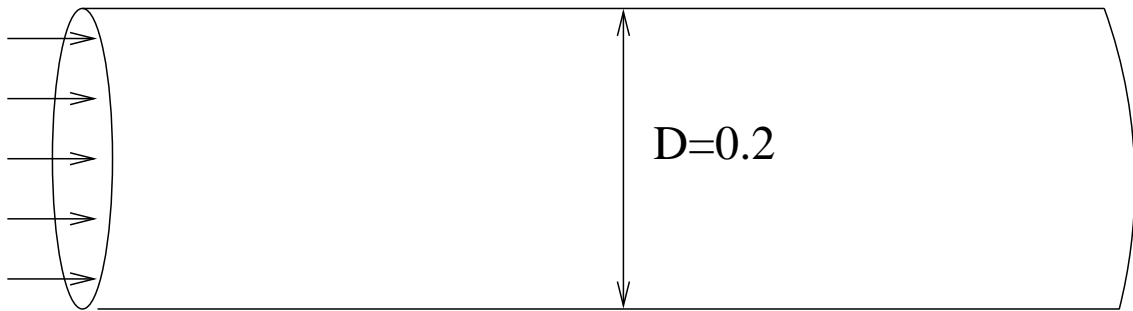
The classroom examples used were:

1. Laminar and turbulent flow in a circular pipe
2. Compressible flow in an axisymmetric nozzle
3. 2D flow past an airfoil

Possible additions for next year:

- Jet
- Flow over cylinder or sphere

## LAMINAR PIPE FLOW

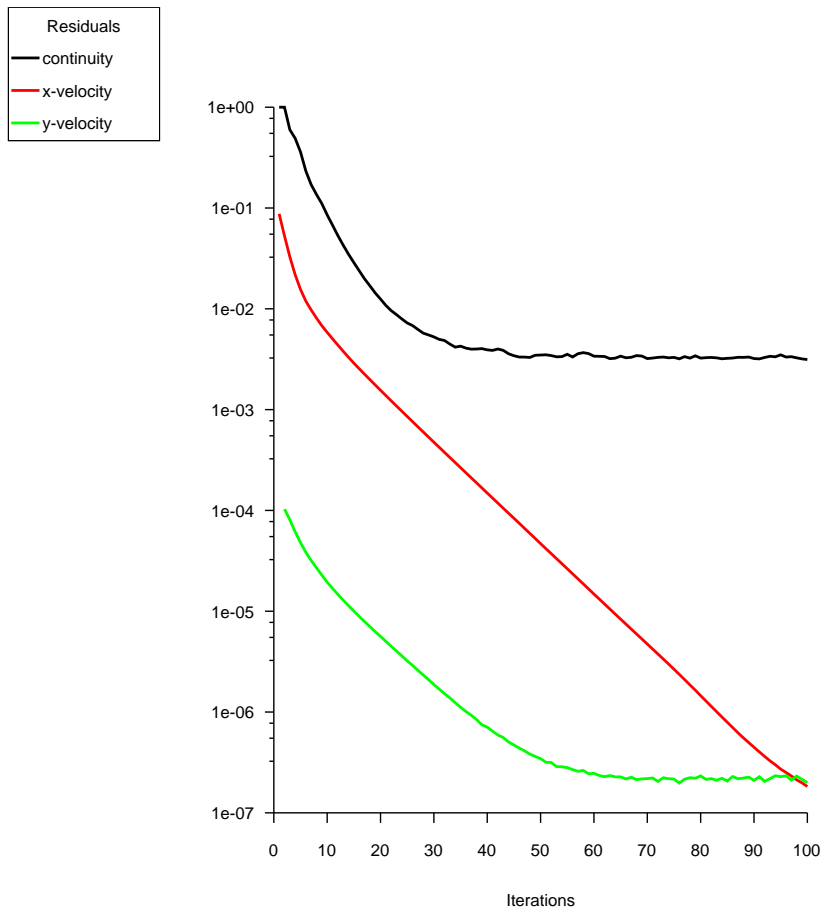


Incompressible, developing flow in a circular pipe.

Inlet velocity = 1 m/s    Exit pressure = 1 atm

$$Re_D = \frac{\rho V D}{\mu} = 100 \text{ or } 200$$

# LAMINAR PIPE FLOW

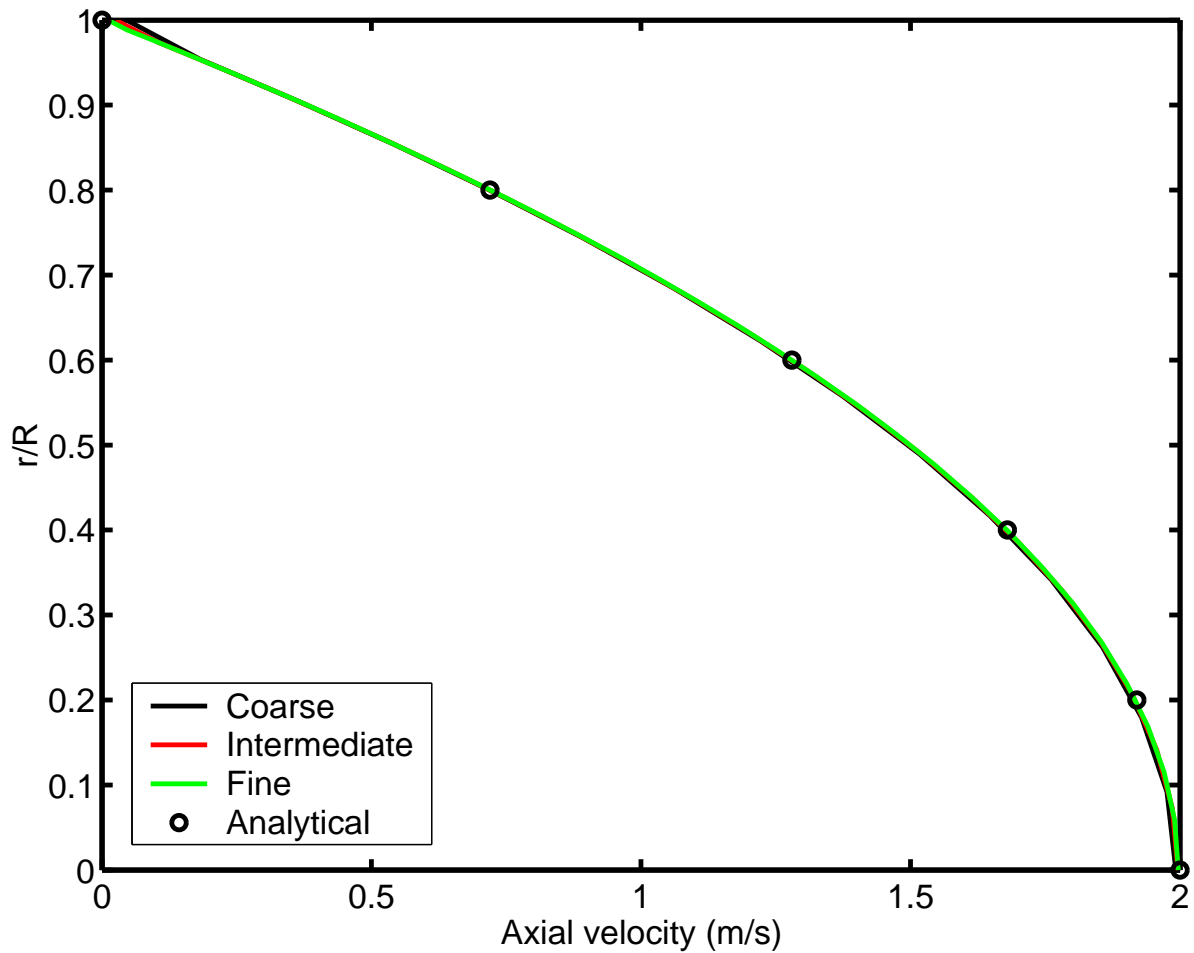


Scaled Residuals

May 30, 2002

FLUENT 6.0 (axi, segregated, lam)

# LAMINAR PIPE FLOW



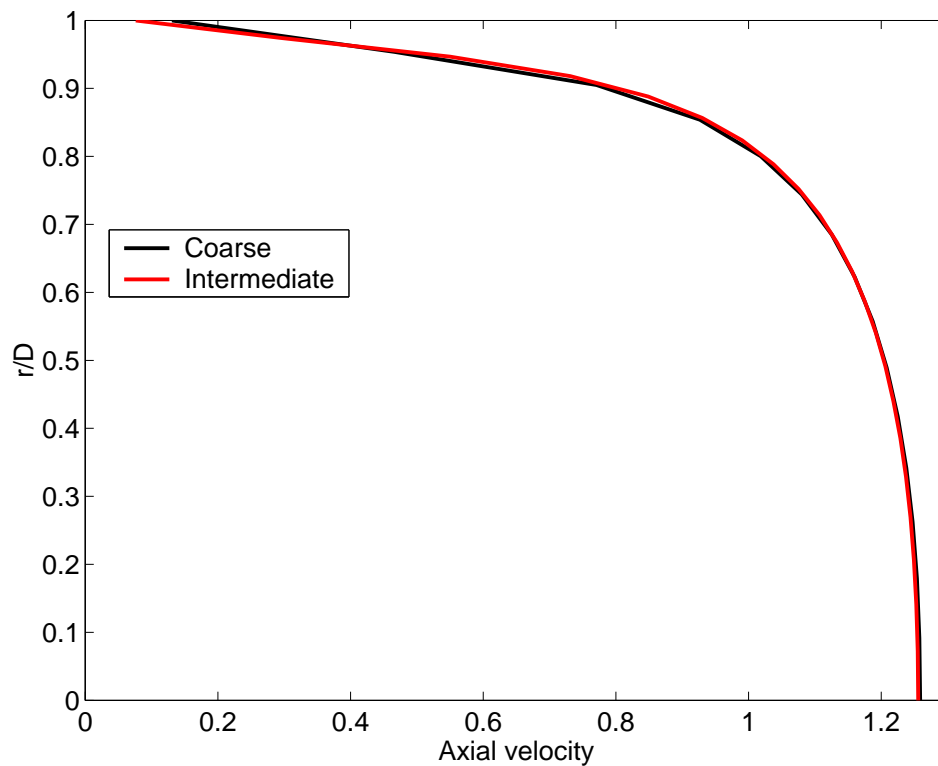
$C_f$  at exit is same as analytical value.

Qualitative discussion of development length

## TURBULENT PIPE FLOW

The Reynolds number is changed to 4,000 and 10,000 by changing  $\mu$ .

Use  $k-\epsilon$  turbulence model (Standard, RNG and Realizable).

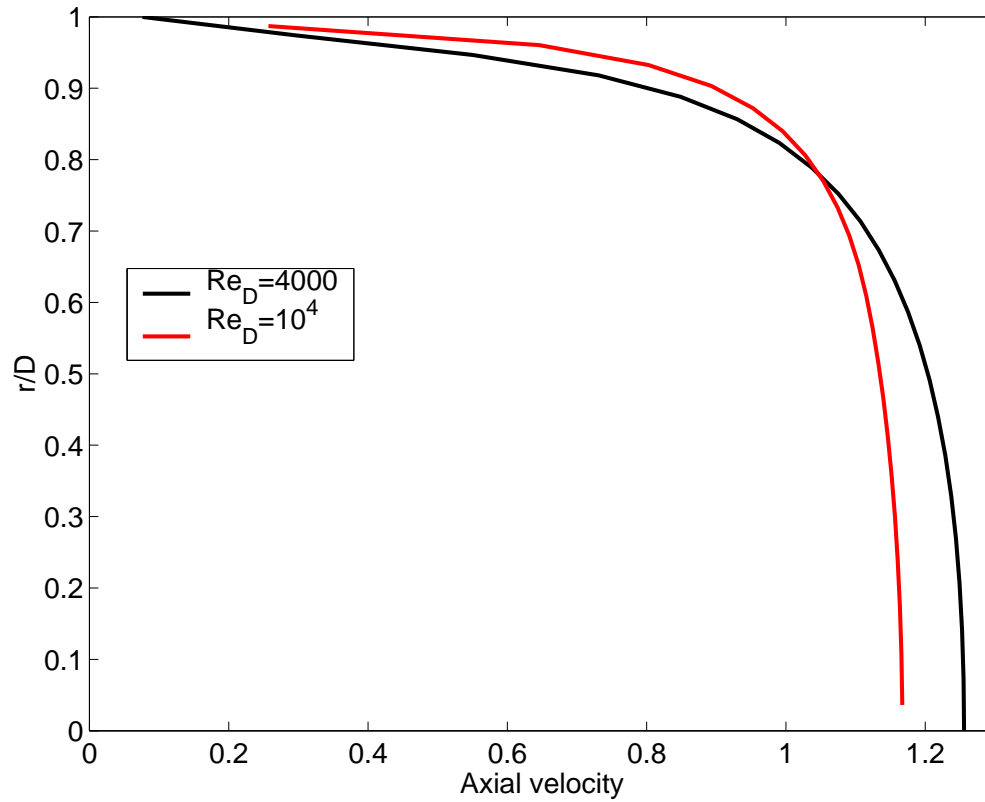


**Std.  $k-\epsilon$ , Intermediate grid,  $Re_D=4000$ :**

$u_{max}=1.26$     White  $u_{max}=1.27$     Diff=-0.8%

$C_f=0.012$     White  $C_f=0.010$     Diff=20%

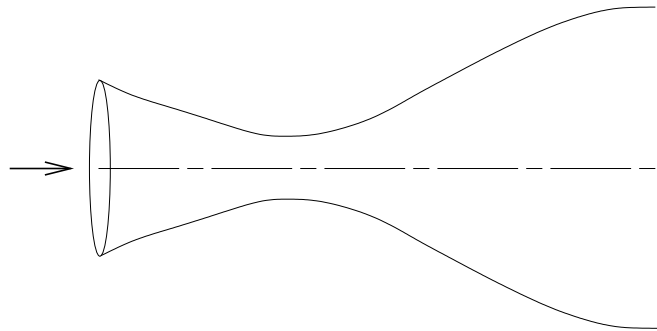
# TURBULENT PIPE FLOW



For  $Re_D = 10,000$ :

|           |           |       |
|-----------|-----------|-------|
| $u_{max}$ | White     | Diff. |
|           | $u_{max}$ |       |
| 1.17      | 1.23      | -4.9% |
| $C_f$     | White     | Diff. |
|           | $C_f$     |       |
| 0.0097    | 0.0077    | 26%   |

## NOZZLE FLOW



Compressible, inviscid flow through an axisymmetric nozzle

Calculation preceded by discussion of 1D nozzle flow analysis.

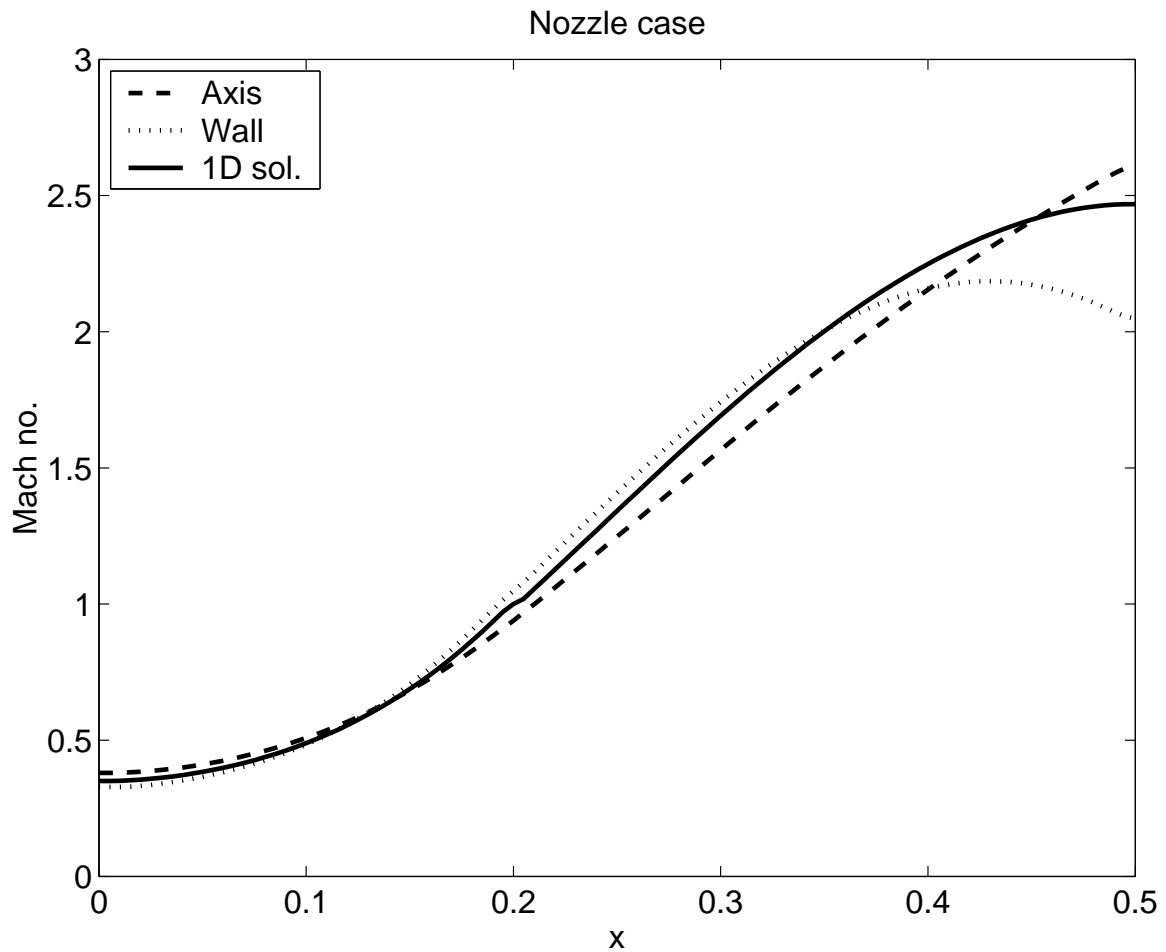
Going from incompressible, viscous to compressible, inviscid flow involves a few clicks of the mouse.

At the inlet,  $p_o=106,439$  Pa     $T_o=300$  K

At the exit,  $p=6,544.7$  Pa

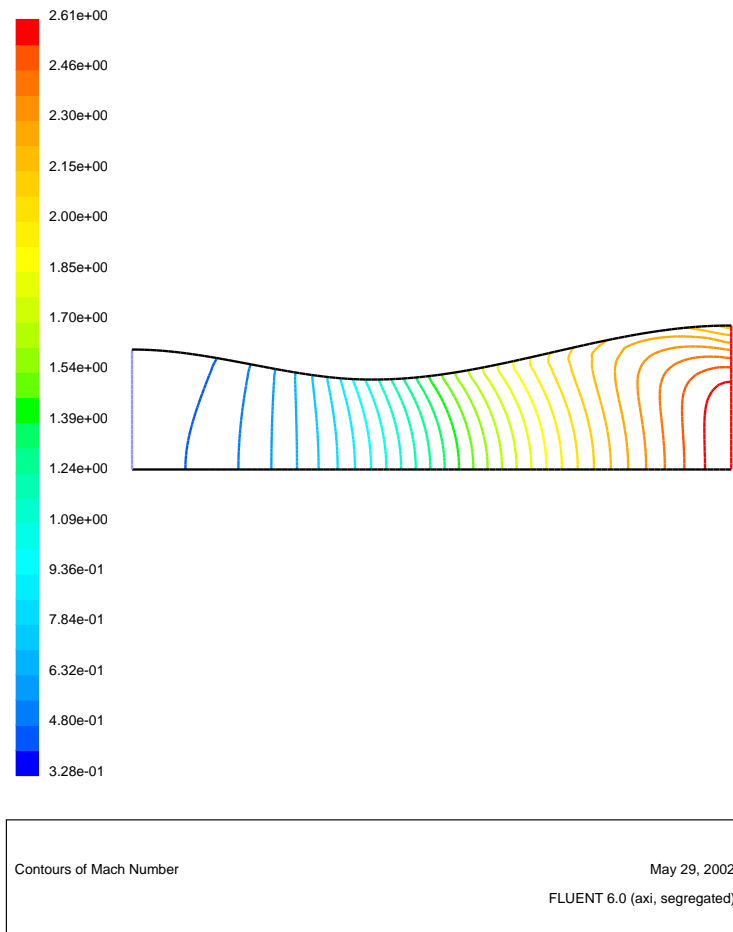
When material is changed to ideal gas, FLUENT automatically turns on the energy equation. Relates to an important physical principle.

# NOZZLE FLOW



- Greatest deviation from 1D result: Wall region near the exit

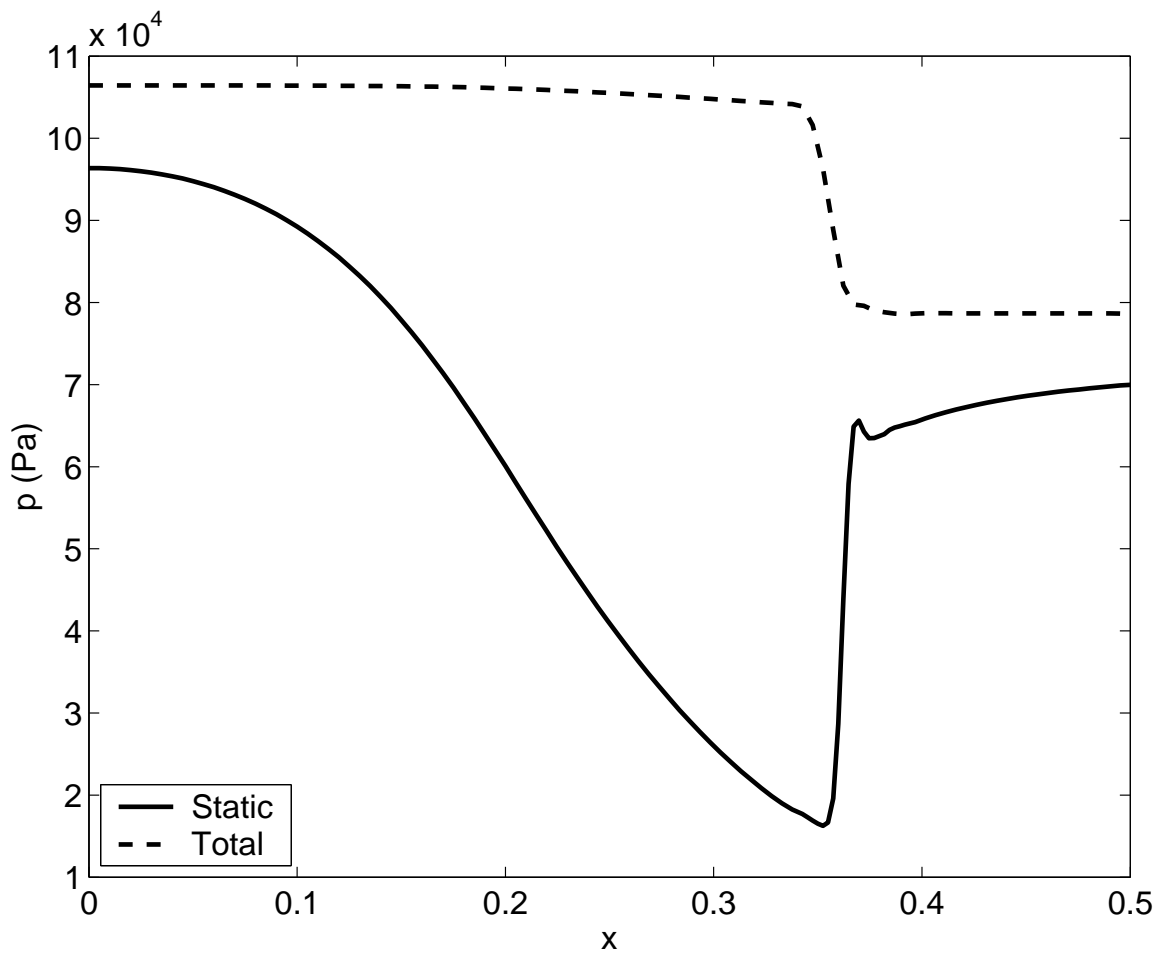
# NOZZLE FLOW



- Flow is strongly 2D in the wall region near the exit.

## NOZZLE FLOW

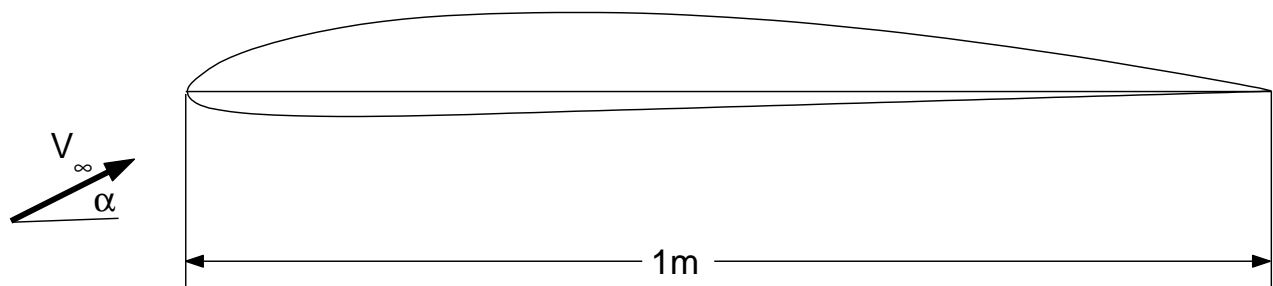
Exit pressure is changed from 6544 Pa to 70,000 Pa.



Shock wave in the diverging section.

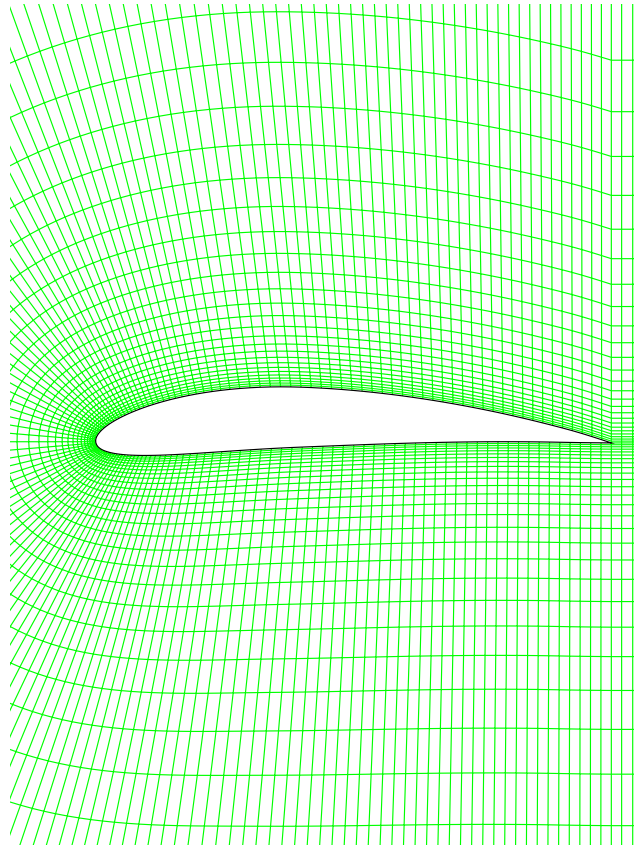
Grid adaption is used to better resolve shock wave.

## AIRFOIL FLOW



- Incompressible flow over an airfoil
- $V_\infty = 50 \text{ m/s}$      $Re = 3.4 \times 10^6$
- Consider both inviscid and viscous cases
- Viscous case: Std.  $k-\epsilon$  turbulence model

# AIRFOIL FLOW

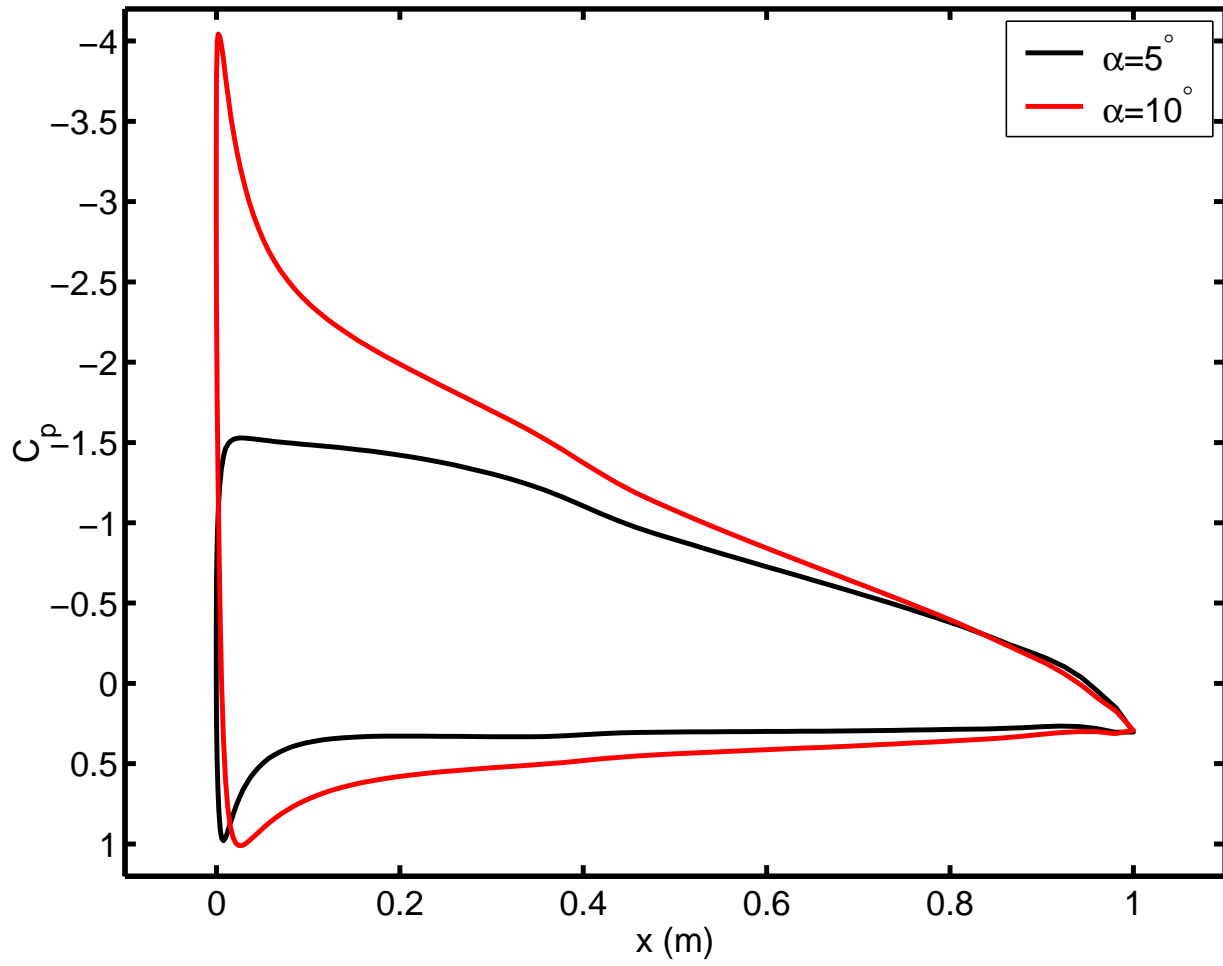


Grid

May 30, 2002  
FLUENT 6.0 (2d, coupled imp)

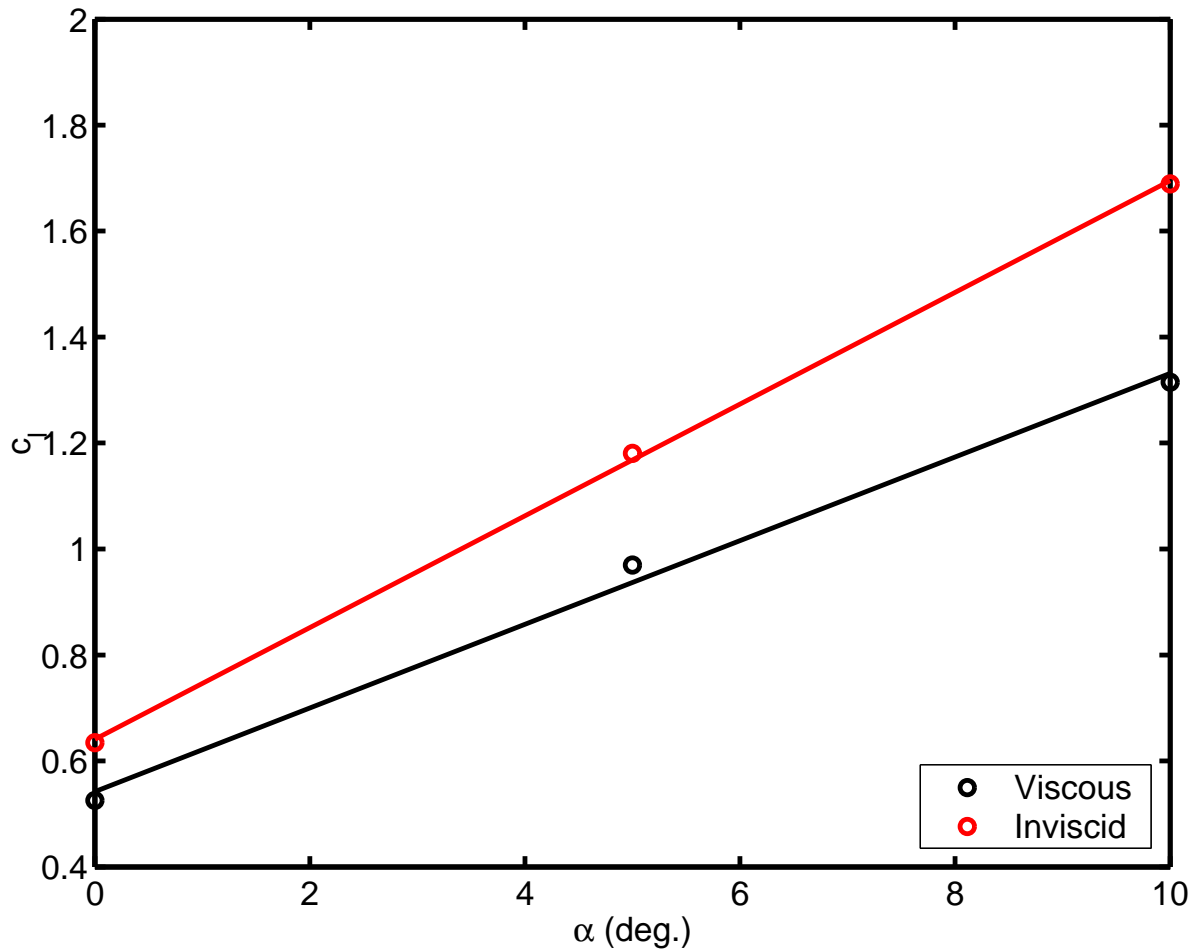
- C-grid with 12,195 cells

# AIRFOIL FLOW



- $c_l \simeq$  Area under curve

# AIRFOIL FLOW



- Inviscid case:  $\frac{dc_l}{d\alpha} = 1.92 \pi$  per radian

- Viscous case:  $\frac{dc_l}{d\alpha} = 1.44 \pi$  per radian

## AIRFOIL FLOW

- Inviscid case:

| $\alpha$   | $c_l$ | $c_d$ |
|------------|-------|-------|
| $10^\circ$ | 1.689 | 0.023 |

- Viscous case:

| $\alpha$   | $c_l$ | $c_{dp}$ | $c_f$    | $c_d$ |
|------------|-------|----------|----------|-------|
| $10^\circ$ | 1.315 | 0.066    | 9.169e-3 | 0.075 |

- These results are with the coupled solver  
Segregated solver gives  $c_d$  values that are about half of the coupled solver

- $c_d$  values are too high

Prof. Caughey's solver:

$$c_l=1.86 \quad c_d=-6 \times 10^{-4} \quad (\alpha=10^\circ, M=0.1)$$

## CONCLUSION

- Need to look into improving the accuracy of FLUENT results.  
University support unable to fully address these concerns.  
Could use help from a senior Fluent engineer.
- Installation could be simplified.
- Exceed X-server is an additional complication.
- Inexpensive student version would be useful.

## CONCLUSION

At the undergraduate level, FLUENT can be a valuable tool in teaching

- The intelligent use of CFD.
- The basic principles of fluid dynamics.

Appropriate curriculum material is needed.  
This effort is a step towards providing this.

Student project ideas solicited.

Positive buzz from students.

Availability of inexpensive, powerful computers and simplified software interfaces enables a new way to teach fluid dynamics.